

Alkaline Sulfite Anthraquinone and Methanol Pulping of Bamboo (*Gigantochloa scortechinii*)

Amin Moradbak,^{a,*} Paridah Md. Tahir,^a Ainun Zuriyati Mohamed,^{a,*} and Rasmina Halis^{a,b}

Alkali ratios and cooking time of the alkaline sulfite anthraquinone (AQ) and methanol (ASAM) pulping process of bamboo (*Gigantochloa scortechinii*) were studied. Bamboo chips were cooked at three different levels of sodium hydroxide and cooking time, namely 14, 16, or 18% for 60, 90, or 120 minutes. Pulping parameters that remained constant were the use of 0.5% ethylene diamine tetraacetic acid (EDTA), with an 80/20 ratio Na₂SO₃/NaOH, 0.1% anthraquinone, 15% methanol, and a temperature of 170 °C in the cooking process. Samples prepared using 14% NaOH and 90 min of cooking time resulted in the highest pulp yield, 52.4%, and a Kappa number of 18.1. It seems that 16% sodium hydroxide and 90 min of cooking time are the most appropriate cooking conditions, giving a 49.1% pulp yield and 14.2 Kappa number. The quality of bamboo pulp produced by the ASAM pulping process was found to be beneficial for the use in paper and board manufacturing.

Keywords: *Gigantochloa scortechinii* bamboo; Fiber dimensions; Chemical composition; ASAM pulping; Pulp properties

Contact information: a: Institute of Tropical Forestry and Forest Products (INTROP) - Universiti Putra Malaysia, 43400 UPM Serdang, Selangor, Malaysia; b: Department of Forest Production, Faculty of Forestry, Universiti Putra Malaysia, 43400 Serdang, Selangor, Malaysia;

* Corresponding authors: ainun.introp@gmail.com; aminmoradbak@gmail.com

INTRODUCTION

The use of non-wood materials in the production of pulp and paper has attracted interest worldwide since 1970 (Saijonkari-Pahkala 2001). Bamboo as a non-wood fiber is a viable alternative source for this kind of industry.

There are more than 70 genera of bamboo available worldwide, and these can be divided into about 1,450 species (Gratani *et al.* 2008). Bamboo species are found in diverse climates, from cold mountains to hot tropical regions. They occur across East Asia, to Northern Australia, and west to India and the Himalayas (Bystriakova *et al.* 2003). They also occur in sub-Saharan Africa, and in the Americas from the Mid-Atlantic United States (Mohlenbrock 1989) to Argentina and Chile, reaching their southernmost point anywhere, at 47°S latitude. Continental Europe is not known to have any native species of bamboo (Levy 1992).

Bamboo is a hygroscopic type of plant, meaning that it is able to obtain water from the environment and hold onto it (Erakhrumen and Ogunsanwo 2009). This is a very good property because, in the chemical pulping processes, cooking liquor needs to penetrate throughout the chips of a sample such as bamboo. Improper penetration of chemicals in the chips may lead to uncooked chip centers, high screen rejects, low pulp yield, and high dirt count. The penetration of chemicals into the chips is considered to take place by two separate processes: 1) mass flow of liquid and solute into the chips and

2) diffusion of solute through the liquid-saturated chip. These two movements act under different processes (Smook 1992; Sixta 2006). The movements of liquid into chips is governed by capillary forces and applied pressure, while the diffusion of chemical into liquid-filled chip is dependent on the concentration gradient between the liquor surrounding the chip and that inside the chip (Smook 1992).

Ogunwusi (2001) noted that the efficiency degree of wood and non-woody fibers to perform excellently in pulp and papermaking is much related to their biometric characteristics. The characteristics such as fiber length, lumen diameter, and fiber diameter may influence the performance of pulp and paper properties, namely bulk, apparent density, and inter-fiber bonding (Dinwoodie 2000). According to Oluwadara and Ashimiyn (2007) fiber length affects paper tear strength. Longer fiber length generally results in stronger paper, which leads to higher tear strength. Lumen diameter influences the effectiveness of beating. Larger lumen diameter of fibers offer better beating effects in comparison to smaller lumen diameter due to the easiness of liquid penetration into both the inner and outer part of fibers as the beating process is being carried out (Smook 1992; Sixta 2006; Reyier 2008).

Patt and Kordsachia in 1986 invented a new pulping process based on alkaline sulfite anthraquinone with methanol pulping known as the ASAM process. Chemical materials that used in the ASAM process are: sodium sulfite (Na_2SO_3), sodium hydroxide (NaOH), anthraquinone (AQ), and methanol (CH_3OH). These materials have key role in places such as sodium sulfite changed lignin to solvable material, AQ has catalytic effects on delignification, and methanol improves the solubility of the AQ (Shukry *et al.* 1999; Knoblauch *et al.* 2000; Miranda and Pereira 2002; Jahan *et al.* 2003; Khristova *et al.* 2002, 2004; Kordsachia *et al.* 2004; Sridach 2010).

Few studies have considered the application of ASAM in the cooking process of both hard and soft wood. Kordsachia *et al.* (1992) reported that *Eucalypt* wood and *E. globulus* had been cooked by ASAM pulping process, which resulted in 56.9% and 53.6% pulp yield, and 14.3 and 10 kappa number, respectively. Pulp yield and kappa number of *Pinus sylvestris* were found to be from 52.9% to 52.5% and 31.8 to 27, respectively (Kordsachia and Patt 1988).

The ASAM pulping process is an alternative cooking process option for kraft and soda pulping processes. Some advantages of ASAM are listed as: avoidance of air pollution, high delignification rate, high brightness of pulp, high pulp yield, and it is easier to bleach the pulps (Kordsachia and Patt 1988; Patt and Kordsachia 1986; Patt *et al.* 1987; Miranda and Pereira 2002).

Parameters with the most significance, which affect delignification and polysaccharide removal, are alkali charge and cooking time (Khider *et al.* 2012a; Mertoglu-Elmas *et al.* 2012). In addition, ASAM pulping process has better selectivity in comparison to kraft or soda pulping processes in terms of delignification, which leads to low kappa number and high viscosity (Knoblauch *et al.* 2000).

The effects of methanol and AQ in this process are: a) stabilization of carbohydrates, b) increased solubility of AQ, c) better penetration of chemical materials into the chips, d) pulp with higher viscosity, and e) better dissolving of lignin. AQ also has effects on pulp yield, increasing delignification, decreasing carbohydrate degradation, and consumption of alkali charge. In other words, AQ has a role of accelerant for dissolution of lignin (Shukry *et al.* 1999; Sixta 2006; Sridach 2010).

AQ and methanol are two additives that can improve the pulp yield by saving polysaccharides. In ASAM, since there are AQ and methanol, pulp can be produced with

high yield, low Kappa number, and suitable paper strengths (Khristova *et al.* 2004). Another advantage of this pulping process is to produce pulp with a low proportion of rejected material. Due to the use of methanol in the cooking liquor, more penetration of chemicals into the chips occurs. Raising pressure of the digester and more air removal of chips are the two main ways of improving the penetration of chemical materials into wood or non-wood chips. Therefore, adding methanol while an ASAM cooking liquor is in the process of penetrating the chips leads to a higher pressure of the digester. As a result, the entrapped air of the chips is displaced, and chemical materials can penetrate into both wood and non-wood chips. Consequently, more delignification happens and fibers can be easily separated (Patt and Kordsachia 1988; Paik *et al.* 1988).

On the other hand, AQ has the role of effective stabilizer in both wood and non-wood polysaccharides. Anthraquinone is effective at extremely lower dosage levels of 0.05 to 0.1% on oven-dry wood, giving good results in most cases (Sixta 2006). Aldonic acid, which is present as a result of isolation from the pulp hydrolyzates, indicates that stabilization takes place through conversion of the end group to the acid out of an oxidation reaction (Fiserova *et al.* 2006; Hart and Rudie 2014). Therefore, according to role of AQ and methanol in ASAM pulping process, one can expect high yields of ASAM bamboo unbleached pulp.

There is no or a little information on ASAM pulping process of bamboo chips. Therefore, the objectives of this study are to investigate the effects of ASAM pulping parameters on bamboo pulp properties.

EXPERIMENTAL

Materials

Gigantochloa scortechinii (bamboo culms), which was used in this study, was collected from 3- to 4-year-old bamboo plants of Pahang state. The whole of the bamboo culms was converted to chips generally within the range 2 to 2.5 cm by a chipper machine at the Universiti Putra Malaysia (UPM). The moisture content of bamboo chips was measured after they had been dried in ambient air.

Methods

Biometric measurement

The Franklin method (1954) was used to determine the biometric characteristic of bamboo such as fiber length, fiber diameter, lumen diameter, and cell wall thickness.

Chemical composition

The bamboo meal for chemical compositions analysis was prepared according to T 257 cm-85 and T 264 cm-97 of TAPPI standards method. The bamboo meal had been passed through BS 40-mesh and collected on BS 60-mesh.

The analysis included ethanol-benzene solvent extractives, hot and cold-water solubility, lignin content, ash content, silicate content, and one percent NaOH solubility based on TAPPI standards method, namely, T 204 cm-97, T 207cm-99, T 222 om-98, T 211 om-93, T 244 cm-99, and T 212 om-98.

Extractive holocellulose

Five grams of air-dried bamboo meal, which had been screened to select particles in the 40 to 60-mesh range, were transferred to a 250 mL Erlenmeyer flask. The bamboo extractive materials were removed using an ethanol-benzene mixture according to T 204 cm-97 of TAPPI standard methods.

Distilled water (160 mL), glacial acetic acid (0.5 mL), and sodium chlorite (1.5 ± 1 g) were added successively. A 25 mL Erlenmeyer flask was inverted in the neck of the 250 mL Erlenmeyer flask and the flask was placed in a water bath, which was adjusted to temperature of 70 to 80 °C in the flask.

The flask was heated for 1 h at the above-mentioned temperature, and the content were mixed by occasional swirling. Then, without cooling, glacial acetic acid (0.5 mL) was added, followed by sodium chlorite (1.5 g). The heating was continued at 70 to 80 °C for an additional hour. At the end of the second and third hours, adding of acetic acid and sodium chloride are repeated respectively. Acid was always added first.

At the end of the third or fourth hour of chlorite treatment, the flask was placed in an ice bath until the contents had cooled below 10 °C. The holocellulose was filtered on a coarse-porosity fritted-glass extraction crucible with a minimum of ice water to transfer all the holocellulose and to remove the color and odor of chlorine dioxide.

Extractive α - cellulose

The holocellulose used for subsequent isolation of α -cellulose was prepared by treating 2 g of bamboo meal OD at 76 °C with 80 mL of buffer solution (48 g sodium hydroxide and 144 g acetic acid) and 2 mL of sodium chlorite solution (27% w/v). 2 mL sodium chlorite solution was added per hour and repeated for five more hours. The holocellulose was filtered and washed with 500 mL of distilled water and 15 mL of acetone, then dried by oven to determine the α -cellulose content.

Pulping of bamboo chips

The ASAM pulping process was conducted in a 5-L digester, which was heated electrically with liquor circulation at three levels of alkali charge and cooking time. The parameters selected included an 80/20 ratio of Na_2SO_3 / NaOH, 15% methanol, 9/1 liquor-to-wood (L/W), and 0.5% EDTA according to Miranda and Pereira (2002), Khider *et al.* (2012a), Khristova *et al.* (2004), and Granholm *et al.* (2010).

Ethylene diamine tetraacetic acid (EDTA) is known as a chelating agent for heavy metal ions such as Mn, Mg, Zn, and Fe. These heavy metals cause some difficulties for the hydrogen peroxide bleaching processes known as totally chlorine free (TCF) and elemental chlorine free (ECF); such problems are generally believed to result from the decomposition of hydrogen peroxide (Colodette *et al.* 1998; Lachenal *et al.* 1997; Yuan *et al.* 1997; Granholm *et al.* 2010). As noted by Gupta (1970), Granholm *et al.* (2010), and Forsskåhl (2000), heavy metals such as iron (Fe) adversely affect the color of pulp and optical properties of the finished paper product. On the other hand, during the cooking the calcium ion can result in scale formation in the digester (Granholm *et al.* 2010). Table 1 shows the cooking conditions for bamboo chips.

Kappa number and freeness of pulp (CSF) of ASAM bamboo pulp were measured based on T 236 om-99 and T 227 om-99 of TAPPI standards method, respectively.

Table 1. Pulp Conditions of ASAM Process of Bamboo

Cooking Code	Chemical materials %					Time (Min)	Temp (°C)	L/W
	NaOH	Na ₂ SO ₃ / NaOH	AQ	EDTA	Methanol			
A1						60		
A2	14					90		
A3						120		
A4						60		
A5	16	80/20	0.1	0.5	15	90	170	9/1
A6						120		
A7						60		
A8	18					90		
A9						120		

NaOH= Sodium hydroxide/Na₂SO₃= Sodium sulfite/ AQ= Anthraquinone/ EDTA= Ethylene diamine tetraacetic acid/Temp= Temperature/ L/W= Liquor to wood ratio

RESULTS AND DISCUSSION

Biometrics Characteristics

Table 2 shows the biometric characteristics of bamboo and other species such as *B. tuda*, *E. globulus*, and cotton stalks.

Average of bamboo fiber length was 1980 µm. The length was the highest among 1890, 840, and 810 µm. The results indicate that bamboo is beneficial to be used in the making of industrial papermaking such as specialty paper (Adamopoulos *et al.* 2007; Strelis and Kennedy 1967; Panshin and De Zeeuw 1980). It is expected that the bamboo's final paper products will have stronger properties. According to Oluwadara and Ashimiyn (2007), longer fiber length contributes to hear tear resistance.

Bamboo has less fiber diameter compared with *B. tuda*, *E. globulus*, and cotton stalks. Kennedy *et al.* (1993) reported that fiber with smaller cells tends to provide lower opacity due to fewer air-fiber interfaces and more fiber-fiber interfaces.

Table 2. Biometric Characteristics of Bamboo and Other Species

Parameters	Species			
	<i>G. scortechinii</i>	<i>B. tuda</i>	<i>E. globulus</i>	Cotton stalks
FL (µm)	1980	1890	840	810
FD (µm)	17.27	17	19	24.98
L.D (µm)	8.66	3.45	10.1	16.75
C.W.T (µm)	3.74	6.78	4.4	4.12
Runkel ratio (2×C.W.T)/L.D)	0.86	3.93	0.87	0.49
Flexibility ratio (L.D/FD) ×100	50.14	20.29	53.15	67.05
Slenderness ratio (FL/FD)	114.64	111.2	44.21	32.42
References	Measured	Sharma <i>et al.</i> 2011	Malik <i>et al.</i> 2004	Tutus <i>et al.</i> 2010

FL= Fiber length/ FD= Fiber diameter/ L.D= Lumen diameter/ C.W.T= Cell wall thickness

As Table 2 shows, bamboo fibers have a suitable lumen diameter, and this has a positive impact on the effectiveness of beating. A larger lumen diameter of fibers offers better beating effects in comparison with a smaller lumen diameter due to the easiness of

liquid penetration in the inner and outer part of fibers during the beating process (Smook 1992; Sixta 2006; Reyier 2008).

High Runkel ratios of fibers generally give rise to stiffer, less flexible, and bulkier paper (Binotto and Nicholls 1977). The results show that bamboo fiber has a similar Runkel ratio in comparison with *E. globulus*. Fiber with higher Runkel ratio could produce paper with greater bulk, *i.e.* a lower apparent density. Kpikpi (1992) noted that the best Runkel ratio to produce higher pulp quality is less than 1.

The flexibility ratio affects fiber-to-fiber bonding, which leads to preferable mechanical paper properties including folding endurance, burst, and tensile index. Since bamboo shows high elastic properties (with a flexibility ratio of 50.14), fibers with 50 to 75 flexibility coefficients have higher elastic properties (Bektas *et al.* 1999). On the other hand, the fiber flexibility coefficients of soft and hardwood are 75 and 55 to 75, respectively (Smook 1992).

Ververis *et al.* (2004) reported that any fiber with less than 70 slenderness ratio is not appropriate to use as a raw material in the wood and paper industry. Therefore, due to the flexibility and slenderness ratios achieved for *Gigantochloa scortechinii*, it is expected that such bamboo will produce pulp and paper with acceptable mechanical properties.

Chemical Composition

The chemical composition of bamboo and other species are shown in Table 3. The ash and silica contents were high but within the range of tropical hardwood, 1 to 3% (Khristova *et al.* 2004). Bamboo chips had high contents of holocellulose and α -cellulose, which were 68.33% and 47.67%, respectively. The ash content of bamboo chips was 1.98%, which is very low when compared with other bamboo species such as *D. hamiltonii*, with 2.6% (Sharma *et al.* 2011).

Table 3. Chemical Composition of Bamboo and Other Species

Factors (%)	Species			
	<i>G. scortechinii</i>	<i>D. hamiltonii</i>	Rice straw	<i>Albizia lebbeck</i>
Ash	1.98	2.6	16.6	1.77
Silica	1.56	-	14.9	0.06
S.E	3.68	2.3	3.5	2.38
1% NaOH	19.82	24.7	49.2	15.64
C.W.S	4.61	3.7	10.7	6.88
H.W.S	5.53	6.7	16.2	7.77
Holocellulose	68.33	73.8	70.9	78.6
Cellulose	47.67	45.1	48.2	46.25
Lignin	26.00	23.9	17.2	25.14
References	Measured	Sharma <i>et al.</i> 2011	Tutus <i>et al.</i> 2004	Khider <i>et al.</i> 2012b

S.E = Solvent extractives (ethanol-benzene)/ **H.W.S** = Hot water solubility/ **C.W.S** = Cold water solubility/ **1% NaOH** = 1% Sodium Hydroxide Solubility

Extractive materials have effects on final pulp yield and brightness. An increase in the percentage of these materials results in decreases of pulp yield and brightness. On the other hand, the consumption of alkali charge is increased (Khristova *et al.* 2004).

According to Robinson (1988), Dutt *et al.* (2004), and Shakhes *et al.* (2011) the amount of cellulose content has a positive effect on mechanical properties of paper. On

the other hand, the pulp yield of chemical pulping is related to contents of cellulose and holocellulose present in the raw material. Therefore, it could be expected that unbleached bamboo ASAM pulp will have high pulp yield according to high cellulose and holocellulose contents.

Bamboo has less lignin content (26%) in comparison to tropical hardwoods (28% to 33%) (Savard *et al.* 1954).

ASAM Pulping Process

ASAM pulping is a type of sulfite pulping that is carried out under alkaline conditions. According to Khristova *et al.* (2002), high pulp yield, high paper strength properties, and easy bleaching in TCF sequences are the greatest advantages of the ASAM pulping process. The ASAM pulping process can be regarded as leading to a combination of the pulp properties of kraft and sulfite processes.

In ASAM pulping with the usage of alkali and sodium sulfite (Na_2SO_3), the depolymerization properties of kraft process and the hydrophilicity-creating properties of sulfite process were illustrated (Shukry *et al.* 1999). In this study, the effect of cooking parameters on bamboo pulp yield, kappa number, and initial CSF have been studied.

Effect of Cooking Parameters on Pulp Yield

According to Fig. 1, the rate of dissolution of bamboo fibers is accelerated based on the increasing alkali charge and cooking time. This shows that the amount of carbohydrate that dissolves during cooking process depends on the alkalinity and effective alkali charge.

At 14% NaOH, the highest pulp yield of ASAM bamboo pulp was measured. Probably the most important type of base degradation is the so-called peeling reaction. The peeling reaction is started from ^2C and the formation of the ketones, which has equilibrium with the corresponding enediols. The next step involves the elimination of the replaced ^4C . This leads to a new formation and reducing end of a dicarbonyl compounds (Sixta 2006). The cellulose chain, which is eliminated, contains a new reducing end. Therefore, this process will be repeated with progressive shortening of cellulose.

Ninety minutes of cooking was found to be the most suitable time to maximize the pulp yield. Overall it occurs as a result of chemical penetration into bamboo chips, which can consequently lead to optimum separation of fibers in the bamboo chips.

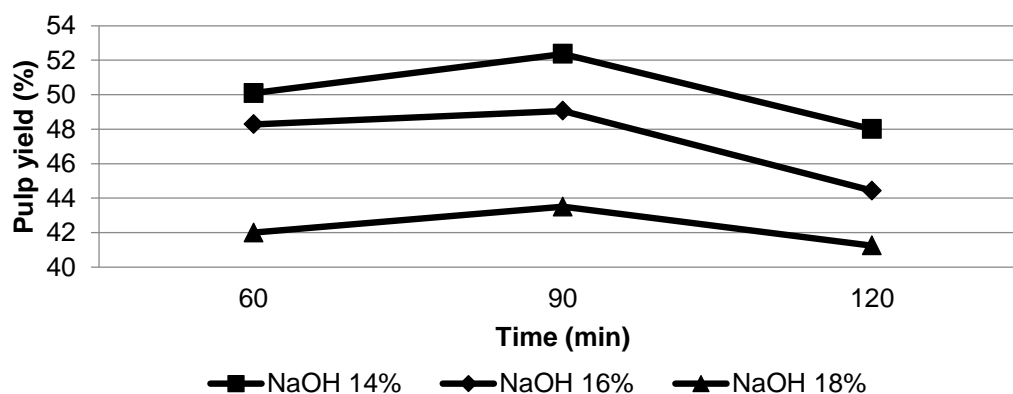


Fig. 1. Relationship between cooking parameters and pulp yield of bamboo

Effect of Cooking Parameters on Kappa Number

The relationship between cooking parameters and kappa number is shown in Fig. 2. At 14% NaOH and 60 min cooking time the highest kappa number was obtained. However, the best cooking time with low kappa number was obtained at 120 min and 18% NaOH. This result occurred due to more penetration of chemical material into the bamboo chips. During the ASAM cooking, methanol increases the pressure inside the digester. Increasing digester's pressure displaces more air from the bamboo chips. By removing air from the chips, cooking liquor can easily penetrate to the materials and more delignification happens.

In addition, as noted by Holton (1977), AQ tends to promote the reduction of the kappa number and increase of the delignification rate. AQ is soluble only in alkali liquor. During cooking time, two formations of AQ occur. If AQ loses one electron, the anthrahydrosemiquinone (AHSQ) is formed, and if it loses two electrons, the anthrahydroquinone (AHQ) is formed. The AHQ is the primary form of AQ that is responsible for delignification. AHQ and quinone methides (QM) of β -aryl ether enter into the procedure afterward.

The mechanism of AQ in the delignification process involves the reduced forms of AQ (particularly the AHQ) reacting with quinone methides (QM) and resulting in β -aryl ether fragmentation and in the improved rate of delignification associated with AQ pulping. The usual mechanism proposes that C-10 carbon of the anthrahydroquinone forms a bond to the C- α carbon of the β -aryl ether dimer. The β -aryl ether and AHQ separate producing a C- α / C- β olefin. Forming the double bond on the styrene-like fragment requires two electrons, oxidizing AHQ back to the AQ starting material (Hart and Rudie 2014).

Therefore, according to the role of AQ and methanol in the ASAM pulping process, AQ can keep the alkali concentration for bulk phase of delignification process. About 60% of the main lignin portion was dissolved in the bulk phase. (Smook 1992; Sixta 2006).

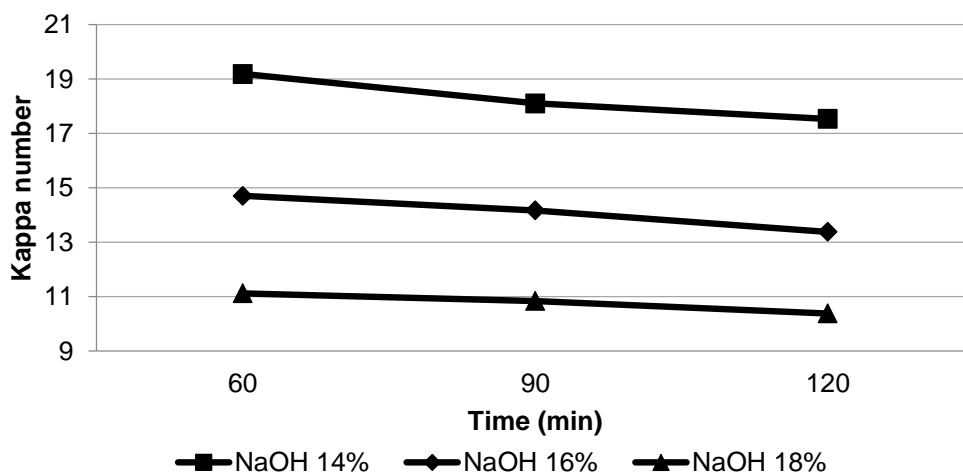


Fig. 2. Relationship between cooking parameters and kappa number of bamboo

Effect of Cooking Parameters on Pulp Freeness

The results show that the highest NaOH led to the lowest fiber freeness. Longer cooking times led to much lower fiber freeness. In alkaline cooking, the middle lamella is removed, and this removal allows the fibrils to extend from the surface of primary wall. When the structure of the fiber is loosened during the cooking, additional water is able to penetrate the fibers. The water is avidly attracted by the available surfaces of the amorphous, hydrophilic hemicellulose material.

Hemicellulose between the elemental threads of the fibers not only provides cleavage planes, but it also attracts water even more strongly than cellulose. Hemicellulose is most responsible for the swelling mechanism (Iwamoto *et al.* 2008; Sun *et al.* 2012; Heijnesson-Hultén *et al.* 2013).

However, besides the possible inclusion of carboxyl groups, hemicellulose is hydrophilic because of the relative shortness of their molecular chains and the presence of a polar group situated at one of their ends.

Therefore, with increasing cooking parameters, more delignification happens, and more fibrils were released on the fiber surface. And also increasing the delignification rate causes more hemicellulose, cellulose, and amorphous materials to be released on the fiber surface. Increasing these materials causes of swelling and increasing mutual bonding. The relationship between cooking parameters and CSF of unbleached bamboo ASAM pulp is shown in Fig 3.

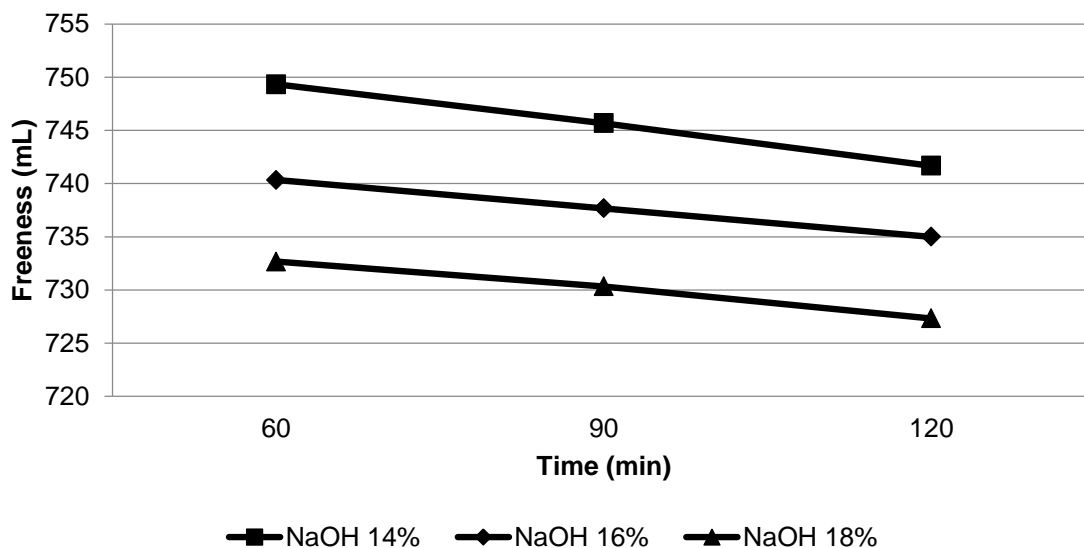


Fig. 3. Relationship between cooking parameters and CSF of bamboo

CONCLUSIONS

1. Based on the findings in this work, the average fiber length of bamboo, of the type studied, is similar to that of softwood. The Runkel, flexibility, and slenderness ratios indicated that the pulp and paper of high quality likely could be produced.
2. The chemical composition of the bamboo, having a 47.67% content of α -cellulose and a 1.98% content of ash, indicates a good potential to produce pulp with suitable yield in comparison with other non-wood species

3. The optimum cooking parameters were found to be 16% NaOH and 90 min cooking time with 49.1% pulp yield and 14.2 kappa number, giving a freeness of 737 mL CSF before refining.

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