

# Production and Detoxification of Inhibitors during the Destruction of Lignocellulose Spatial Structure

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Lignocellulosic biomass is a renewable resource that is widely abundant and can be used to produce biofuels such as methanol and ethanol. Because biofuels have the potential to alleviate shortages of energy in today's world, they have attracted much research attention. The pretreatment of lignocellulose is an important step in the conversion of biomass products. The pretreatment can destroy the crosslinking effect of lignin and hemicellulose on cellulose, remove lignin, degrade hemicellulose, and change the crystal structure of cellulose. The reaction area between the enzyme and the substrate is enlarged, and the yield of subsequent enzymatic hydrolysis and microbial fermentation products is significantly increased. Conventional pretreatment methods help convert lignocellulosic material to sugars, but the treatments also produce some inhibitors, which are mainly organic acids, aldehydes, phenols, and other substances. They may affect the subsequent saccharification and growth of fermentation microorganisms, thereby reducing the bioconversion of the lignocellulose. It is therefore necessary to take effective means of detoxification. This paper reviews lignocellulose pretreatment methods, with an emphasis on inhibitors and their management. A summary is provided of detoxification methods, and the future use of lignocellulosic biomass for fuels prospects.

DOI: 10.15376/biores.17.1.Luo

Keywords: Pretreatment; Inhibitors; Detoxification

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## INTRODUCTION

In the era of rapid development of industrialization, mankind's demand for energy is increasing. Shortages are anticipated in oil, coal, natural gas, and other resources, and pollution-related energy usage can lead to serious ecological environment problems. Vigorously developing renewable energy is of great significance for avoiding the usage of fossil fuels and improving the ecological environment. Lignocellulosic biomass is the only predictable sustainable resource in the world that can provide humans with materials and fuels. It has abundant reserves and wide sources, which can effectively overcome the oncoming shortage of traditional fuels (Raud *et al.* 2016; Valdivia *et al.* 2016). In recent years, research on the pretreatment of wood fiber and bioenergy conversion technology of its products has attracted continuous attention at home and abroad (Xavier *et al.* 2010). Biomass resources are widely distributed on the earth and are dozens of times as much as fossil energy, but their development is slow due to a low utilization rate. Common lignocellulosic substances include waste rice husk, straw, poplar sawdust, *etc.* (Yu *et al.*

2018). Due to the complex chemical structure of lignocellulose, the components of cellulose, hemicellulose, and lignin are cross-linked with each other, and it is difficult to separate the components under normal conditions, which affects the conversion of lignocellulose to biomass fuels. The limitation is that only in the presence of a catalyst will it be hydrolyzed into sugars (Rastogi and Shrivastava 2017), and then microbial fermentation and other methods can be used to produce the required products (Bajwa *et al.* 2011).

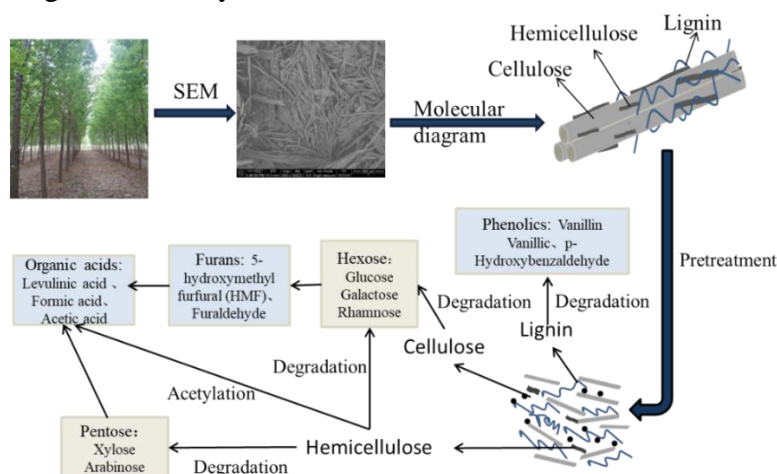
## LIGNOCELLULOSIC PRETREATMENT METHODS

### Basic Composition of Lignocellulose

Lignocellulose is composed of three main components: cellulose, hemicellulose, and lignin (Koddenberg 2016), and the biotransformation process is shown in Fig. 1. Among them, cellulose is composed of glucose through glycosidic bonds, and its properties are relatively stable (Abdelaziz and Hulteberg 2017).

Hemicellulose is a branched heteropolysaccharide, of which different versions are composed of xylose, arabinose, galactose, glucose, mannose, *etc.*, which can carry acetyl groups (Cullis and Mansfield 2010). It is interconnected with cellulose to form a hard network. The hemicellulose structure contains branched chains, so the crystallinity is lower and more unstable, and it is more prone to degradation (Emmel *et al.* 2003).

Lignin is a high-molecular amorphous polymer formed by three phenylpropane units connected to each other in a non-linear manner (Diwan *et al.* 2017). Usually, lignin is mainly located between hemicellulose and cellulose (Emmel *et al.* 2003), which constitutes a lignin-carbohydrate complex, provides structural support, and plays a role in resisting pressure. The higher the proportion of lignin, the less likely it is to be degraded by chemical reagents and enzymes.



**Fig. 1.** A schematic view of a lignocellulosic conversion process

### Types of Pretreatment

Through the pretreatment of lignocellulose, the structure is damaged to varying degrees, which is beneficial to hydrolysis. According to a single preprocessing method or a combination of multiple methods, the preprocessing can be divided into traditional preprocessing and new preprocessing classification. Table 1 lists common pretreatment methods.

**Table 1.** Pretreatment Methods and Influence on Lignocellulose

Type of Preprocessing	Method	Common Reagents	Main Influence	References
Traditional Pretreatment	Physical method: Mechanical pulverization, Extrusion, Grinding and milling)	None	Reduce lignocellulose particle size	Xu <i>et al.</i> 2016;
	Chemical method (Acid, Alkaline Organosolv method)	HCl, H <sub>2</sub> SO <sub>4</sub> , CH <sub>3</sub> COOH, NaOH, KOH, Ca(OH) <sub>2</sub> , Ammonia, Methanol	Ester bonds between lignin and hemicellulose, hydrogen bonds between the cellulose and hemicellulose are broken, the amorphous structure into wood fiber arrangement	Song <i>et al.</i> 2014; Tang <i>et al.</i> 2017; Hyung <i>et al.</i> 2021
New Pretreatment	Steam explosion	None	Arrangement structure destruction and degradation of lignocellulose hemicellulase	Yoo <i>et al.</i> 2011; Borand <i>et al.</i> 2020
	Alkaline hydrogen peroxide method	H <sub>2</sub> O <sub>2</sub> , O <sub>3</sub> -NaOH, NaOH-Urea	Removal of lignin	Liu and Li 2017; Huang <i>et al.</i> 2020
	Cellulose solvent and organic solvent combination	Ethanol concentrated phosphoric acid	Crystallinity of Lignin	Mielenz <i>et al.</i> 2007
	Electro-chemistry	Electrochemical Oxidation (ECO) and Biodegradation	Destroy the refractory bonding structure of lignin	Huang <i>et al.</i> 2012; Cui <i>et al.</i> 2015

### Traditional Pretreatment Methods

Mechanical pulverization is a commonly used physical method. It mainly reduces the size of lignocellulose particles through traditional mechanical pulverization and makes them loosely arranged to increase the reaction area between lignocellulose and subsequent reagents, thereby improving utilization efficiency. However, mechanical pulverization only has the effect of reducing the size of lignocellulose particles, without destroying the chemical structure of lignin, and has almost no effect on the degradation of hemicellulose and lignin (Zeng *et al.* 2007; Xu *et al.* 2016).

Acid pretreatment is a relatively mature pretreatment method of biomass energy. It usually takes concentrated or dilute acid (Emmel *et al.* 2003; Karapatsia *et al.* 2017). Under certain temperatures and pressure, acid molecules will break the glycosidic bond between cellulose and hemicellulose, thereby partially or completely hydrolyzing hemicellulose into monosaccharides, leading to the destruction of the structure of lignocellulose (Tan

2015). In the pretreatment process, when the acid concentration is more than 10%, it is regarded as concentrated acid, the temperature is usually less than 100 °C, the dilute acid concentration is usually less than 5%, and the reaction temperature is relatively high, *i.e.* 100 to 240 °C (Jönsson and Martín 2016). Acid pretreatment has been widely used due to its low cost, rapid reaction, and good treatment effect, but it has the disadvantage of strong corrosiveness (Hang *et al.* 2021). Song *et al.* (2014) used 1% H<sub>2</sub>SO<sub>4</sub>, 2% HCl, 3% H<sub>2</sub>O<sub>2</sub> and 4% CH<sub>3</sub>COOH to pretreat corn stalks at 100 °C for 7 days and then produce methanol. The yields were increased by 62.4%, 74.6%, and 44.2%, respectively, compared with the untreated. Geddes *et al.* (2010) treated sugarcane with dilute phosphoric acid at 160 °C, and the degradation rate of hemicellulose was greatly improved. However, in the process of acid hydrolysis, lignocellulosic will produce a large number of inhibitory substances that affect the subsequent fermentation, which restricts the development of the fuel industry and related industries (Zaldivar *et al.* 2000).

Alkaline pretreatment is also widely used in the pretreatment process. Compared with acid treatment, it is relatively mild (Silverstein *et al.* 2007; Kamran *et al.* 2020). Commonly used alkaline reagents include NaOH, Ca(OH)<sub>2</sub>, KOH, and ammonia. Alkaline pretreatment successfully removes lignin from biomass by destroying the biomass. The OH<sup>-</sup> ion can destroy lignin and xylan, ester bonds between hemicellulose, and other components, thus increasing the porosity of lignocellulose and reducing its crystallinity (McIntosh and Vancov 2010). These changes favor an amorphous wood fiber structure, thereby reducing the crystallinity and polymerization degree of cellulose. Among the commonly used alkaline reagents, NaOH is the most studied and the most common (Chen *et al.* 2012). An *et al.* (2021) used 2% NaOH to pretreat at 121 °C for 10 minutes, as well as enzymatic hydrolysis. The glucose content (GC) and enzymatic hydrolysis degree (ED) were 46.7% and 55.3%, respectively. After being pretreated with NaOH, it was 2.4 times and 2.5 times higher than the control (untreated). Continuing to use *Saccharomyces cerevisiae* K35 for ethanol fermentation, the results showed that the highest ethanol yield can reach 41.3 g, which is 2.4 times higher than that of the control group. Jiang *et al.* (2020) studied the pretreatment of reeds with NaOH and Ca(OH)<sub>2</sub>. The highest sugar yields of NaOH and Ca(OH)<sub>2</sub> pretreatment were 44.9% and 25.8%, respectively. These were 85% and 70% higher than untreated giant reeds, respectively.

The hydrothermal method is a kind of green pretreatment method. Robinson *et al.* (2015) used hot water to pretreat bagasse and bamboo at different temperatures and different times, and after optimization, the reducing sugar content reached 26.5 and 17.98 g/L, respectively. Harahap and Kresnowati (2018) used oil palm empty fruit bunch (OPEFB) as raw material to prepare xylitol and autohydrolysis at 1.5 barg/127.9 °C for 60 minutes to obtain the best yield. The yield of xylose was 0.085 g xylose/g OPEFB. At the same time, because of its natural pH, the hydrolysate can be used directly as a fermentation substrate. Meilany *et al.* (2020) used oil palm empty fruit bunches (OPEFBs) as raw materials; the effects of different pretreatment processes on the sugar recovery of lignocellulosic biomass were studied. The hydrothermal process was used to enzymatically hydrolyze OPEFB. The effects of temperature, solid-phase loading, and pretreatment time on the hydrothermal of OPEFB were investigated. The concentration of xylose in the hydrolysate of OPEFB was analyzed by high-performance liquid chromatography. The results showed that the pretreatment time for maximum xylose recovery was 165°C, and the xylose recovery rate of pretreated OPEFB was 0.061 g/g (35%)

The organosolv method is also commonly used as a pretreatment method. Lignin can be effectively dissolved by organic solvents (Mesa *et al.* 2011). After the material is

pretreated, it is recycled and reused by distillation, and the pretreated product can be used as a chemical raw material (Hamidah *et al.* 2017). Zhang *et al.* (2018) under the conditions of 120 °C, 10 min, and microwave irradiation, used methanol/dioxane binary solvent pretreated poplar while achieving over 99% of conversion of enzymatic saccharification. Amiri *et al.* (2014) used rice straw as raw material, pretreated with 1% sulfuric acid in 75% ethanol aqueous solution at 150 °C for 60 min, and the total enzymatic sugar concentration was as high as 31 g/L. Compared with alkaline pretreatment, the lignin dissolved by ethanol had less structural degeneration and a more uniform molecular weight. However, organic solvents such as ethanol have the disadvantages of high volatility, high temperature, high requirement for equipment, and a long time requirement (Tang *et al.* 2017).

### New Pretreatment Methods

The disadvantages of traditional pretreatment methods are long times, high equipment requirements (Chin *et al.* 2020), high economic cost, low enzymatic hydrolysis efficiency, and the fact that they may cause a certain degree of corrosion of the instrument. Therefore, some new pretreatment methods have been developed and utilized. The conditions employed are relatively mild in these new pre-treatment methods, which implies low equipment requirements. In addition, there have been improvements in efficiency and the hydrolysis reaction period had been shortened.

Steam explosion takes place at high temperature and pressure. the rapid heating method using saturated steam dissolving lignocellulose, broad applicability, is an environmentally friendly pretreatment (Yoo *et al.* 2011; Ewanick and Bura 2011; de Albuquerque Wanderlay *et al.* 2013). It can damage the structure of the arrangement and degrade the hemicellulose component of lignocellulose, thus effectively improving the efficiency of enzymatic hydrolysis and enhancing the conversion efficiency (Martín-Sampedro *et al.* 2012; Yu *et al.* 2020; Cubas-Cano *et al.* 2020). For example, Borand *et al.* (2020) used pine to conduct steam explosion treatment at 190 °C for 10 min, and the final glucose yield was 97.7%, whereas xylose, mannose, galactose, and arabinose were 85.6%, 87.8%, 86.4%, and 90.3%, respectively. He *et al.* (2019) used steam explosion pretreatment at a pressure of 1.5 MPa to pre-treat seabuckthorn; it was found that a reaction of 20 minutes could remove 77.2% of hemicellulose, and the sugar yield after enzymatic hydrolysis was 4.54 times that of the untreated control.

Alkali hydrogen peroxide pretreatment (AHP) is one of the most promising pretreatment methods (Liu *et al.* 2017). AHP mainly uses H<sub>2</sub>O<sub>2</sub> to remove lignin in an alkaline medium, while increasing the dissolution of hemicellulose. The degree of dissolution depends on the pH of the reaction. Chen *et al.* (2020b) established an improved method of analytic hierarchy process (AHP) for delignification; at 100 °C the removal percentage of lignin reached 80.0%, which was higher than the 74.9% level that was achieved in the pretreatment without ethanol. The effect of alkaline hydrogen peroxide (AHP) pretreatment on bamboo stalk and bamboo stalk structure changes and enzymatic hydrolysis was studied. The results showed that after AHP pretreatment, compared with the chemical composition of raw materials, cellulose increased by 36.9%, hemicellulose decreased by 50.7%, lignin decreased by 37.9%, and 370 mg/g reducing sugars were obtained after enzymolysis (Nasir *et al.* 2020).

Wang *et al.* (2018) used ozone-NaOH combined pretreatment of corn stover to achieve a removal percentage of lignin up to 84.4%, which could not only reduce the amount of NaOH but also achieve a maximum enzymatic hydrolysis efficiency of up to

91.7%. Dai *et al.* (2015) adopted the pretreatment method combining bacteria with NaOH-urea to improve the enzymatic hydrolysis performance of the rice straw. The results showed that combined pretreatment increased the yield of reducing sugar and glucose by 1.40 and 1.37 times, respectively, compared with single pretreatment.

The method of combining organic solvent and cellulose solvent has been applied for pretreatment. Zhang *et al.* (2007) treated rice straw with ethanol and concentrated phosphoric acid under the condition of atmospheric pressure and 50 °C, which could greatly break the crystallinity of lignin, make the substrate become irregular, and remove hemicellulose, thus improving the efficiency of enzymatic conversion. Compared with a single pretreatment method, it greatly reduces the number of enzymes used, and the enzymatic hydrolysis time is significantly reduced, which has good application value.

Electrochemistry is a method that uses the phenomena of charged interfaces between conductors and the changes that occur (Huang *et al.* 2012). Electrochemical pretreatment can destroy the refractory bonding structure of lignin, which is an economical and effective method for lignin degradation. This process has mild reaction conditions, no need to add chemicals, and the ability to be used over a wide range. Accordingly, it can be regarded as a green pollution-free pretreatment process. Cui *et al.* (2016) proposed a technology for synergistic degradation of lignin that combines electrochemical oxidation (ECO) and biodegradation (BD). The results showed that after ECO treatment, the biodegradability of lignin increased from the range 0.20-0.25 to 0.31-0.37. As a result, the subsequent biodegradation time was reduced. However, the technology is not mature enough and is currently in the laboratory stage. Future research of this technology is needed to establish and improve the electrochemical pretreatment technology so that it can be used in industrial production.

### **Inhibitor Production during Pretreatment and their Inhibitory Effects**

Lignocellulosic substances will produce a series of low-molecular-weight fermentation inhibitors during the hydrolysis process (Hidayatullah *et al.* 2020). Table 2 shows several common types of inhibitors, which seriously affect the fermentation and utilization of substrates by microorganisms.

### **Inhibition Mechanism of Acids**

Formic acid, acetic acid, and a small amount of levulinic acid is a common combination of inhibitory substances (Parawira and Tekere 2011). The main formation mechanism of these inhibitors is that acid can degrade hemicellulose, which generates pentylene under the action of acid. Sugar, acetic acid (Ravindran and Jaiswal 2016), pentoses, and hexoses are dehydrated to form furfural and 5-hydroxymethylfurfural (5-HMF) (Wang *et al.* 2019; Cola *et al.* 2020). 5-HMF and furfural will decompose with the generation of formic acid (van der Pol *et al.* 2014; Chen *et al.* 2019). Studies have shown that under the same pH value, formic acid has a lower pKa value than acetic acid and levulinic acid, and the degree of dissociation of formic acid is also smaller than that of acetic acid and levulinic acid. It is easy to enter the cell membrane in molecular form and inhibit microbial activity. Therefore, the toxicity of formic acid is higher than that of acetic acid and levulinic acid (Hyland *et al.* 2013). Generally, there will be no separate acid inhibitors, and if furan aldehydes are or phenols are present, they would inhibit the enzyme activity; in addition, the presence of microorganisms (Li *et al.* 2016) would influence enzymatic hydrolysis and fermentation.

**Table 2.** Types, Sources, and Inhibitory Effects of Inhibitors

Pretreatment methods	Types of Inhibitors	Common Inhibitors	Source	Main Influence	References
Acid pretreatment Alkaline pretreatment Organosolv method Steam explosion pretreatment Liquid hot water pretreatment	Acids	Formic acid, acetic acid and a small amount of levulinic acid	Hemi-cellulose	Inhibition of the activity of microorganisms and enzymes, enzymatic hydrolysis and fermentation effect	Parawira and Tekere 2011; Li <i>et al.</i> (2016)
Alkaline pretreatment Steam explosion pretreatment Liquid hot water pretreatment	Phenols	Vanillin, syringaldehyde, vanillic acid, <i>etc.</i>	Lignin	Inhibiting the normal growth of microbial cells and fermentation efficiency	Varga <i>et al.</i> 2004; Moreno <i>et al.</i> 2012
Acid pretreatment Organosolv method Steam explosion pretreatment Liquid hot water pretreatment	Aldehydes	Furfural and 5-Hydroxymethyl-furfural	Cellulose Hemi-cellulose	Inhibit the normal metabolic activity of microorganisms	Moreno <i>et al.</i> 2012; Iwaki <i>et al.</i> 2013
Ionic liquids pretreatment	Metal ions	Iron, copper	External equipment	Inhibit microbial activity metabolizing enzymes	Mussatto and Roberto 2003

### Inhibition Mechanism of Phenolic Substances

Phenolic substances in lignocellulosic pretreatment solution are mainly lignin degradation products, usually aromatic compounds containing a benzene ring. There are dozens of phenolic substances identified now (Viegas and Sá-Correia 1991; Varga *et al.* 2004). Although the content of phenolic substances is relatively low, the inhibition effect is more serious and affects the subsequent fermentation of hydrolysate (Palmqvist and Hahn-Hägerdal 2000). Even at low concentrations, phenolics exhibit very strong inhibition of fermentation (Chen and Dou 2016). Examples include vanillin, syringaldehyde, and vanillic acid, which provide the most significant inhibition of fermentation (Moreno *et al.* 2012). Compared with acid substances, vanillin in the concentration of 4 g/L completely inhibits the sugar utilization in *Saccharomyces cerevisiae*, and 6 g/L completely inhibits ethanol fermentation (Soudham *et al.* 2014). Heipieper phenolic compounds have been found to have an important impact on fermentation, and the explanation is that the material can infiltrate into the cell membrane and destroy the integrity of the cell membrane; this

inhibits the normal growth of microbial cells, hurts fermentation efficiency, and reduces the efficiency of the fuel ethanol (Yi *et al.* 2015; Chen *et al.* 2020c). Different from weak acids and furan aldehydes, phenolic substances not only significantly inhibit the growth of microorganisms, but also significantly reduce the activities of cellulase and hemicellulase (Taherzadeh *et al.* 2000; Rahikainen *et al.* 2017).

Phenolic substances are the most significant inhibitors of inhibition in enzymatic hydrolysis or microbial fermentation, and the molecular weight and the position of substituents (*meta*-position, *ortho*-position, *para*-position) are important factors that affect the inhibition effect of phenolic substances (Qin *et al.* 2016; Ishida *et al.* 2017). Generally speaking, the lower the molecular weight, the higher the toxicity (Ladeira Ázar *et al.* 2017).

### **Inhibition Mechanism of Aldehydes**

The aldehyde inhibitor category consists of furfural and 5-HMF (Field *et al.* 2015), which are the by-products of lignocellulosic pretreatment liquid having the greatest content and the highest toxicity. They are furan derivatives of five-carbon sugars and six-carbon sugars. They enter cells by means of active transport and have little inhibition of cellulase, mainly inhibiting the growth of microorganisms (Palmqvist *et al.* 1999). Studies have shown that furfural and HMF can affect intracellular respiration and thus affect the glycolytic pathway *in vivo* (Iwaki *et al.* 2013). Sárvári *et al.* (2003) believed that *Saccharomyces cerevisiae* could reduce furfural to furfuryl alcohol. Such a reduction process is expected to cause a large amount of consumption of coenzyme NADH, leading to an imbalance in xylose metabolism. Antioxidant proteins are also inactivated due to the reduction of available coenzymes, making yeast cells vulnerable to oxidative damage (da Silva *et al.* 2017). The work of Jung *et al.* (2019) showed that when only furfural or HMF was present, the ethanol yield of the final fermentation was less affected. Some studies have shown that when furfural and HMF are both present, the normal metabolic activities of microorganisms are inhibited, thus reducing the ethanol yield in the fermentation process (Iwaki *et al.* 2013). In addition, furfural can also lead to the accumulation of reactive oxygen species in yeast (reactive oxygen species, ROS), resulting in damage to the cell nucleus and may even induce cell death (Song *et al.* 2017).

### **Inhibition Mechanism of Metal Ions**

In the pretreatment process of lignocellulose, due to corrosion of mechanical equipment or added chemical substances, some metal ions will be solubilized, such as iron and chromium. These ions will inhibit the activities of metabolism-related enzymes of microorganisms, and they are not conducive to the growth and fermentation process of microorganisms (Mussatto and Roberto 2003).

### **Detoxification of Inhibitors**

The inhibitors in the lignocellulose pretreatment liquid seriously affect the subsequent enzymatic hydrolysis and saccharification process of enzymes and microorganisms, which is also one of the main difficulties in the comprehensive utilization of lignocellulose. Therefore, effective measures must be taken to reduce or remove the negative effects of inhibitors and improve the utilization rate of lignocellulose, in order to achieve large-scale production of biomass energy. In recent years, scholars throughout the world have tried various methods around how to get rid of inhibitors and made some new



progress. As shown in Table 3, the approaches employed can be divided into chemical, physical, biological, and integrated detoxification methods.

**Table 3.** Common Detoxification Methods and Their Advantages and Disadvantages

Type of Removal	Detoxification Method	The Main Advantage	Main Disadvantage	References
Physical method	Adsorption, membrane filtration and extraction	Furan aldehydes, acetic acid and formic acid can be removed	Loss of a large sugar	Keshav <i>et al.</i> 2016
Chemical method	Alkali, reducing agent, persulfate method	Most furan aldehydes, phenols, and weak acid species removed	Large quantities of reagents, and cannot be recovered, a smaller range of detoxification, lower specific	Yayun <i>et al.</i> 2016; Zhou <i>et al.</i> 2021
Biological law	Enzyme microorganism	Mild conditions, low loss percentage sugar	Long reaction cycle Time was needed	Saravanakumar <i>et al.</i> 2016; Tramontina <i>et al.</i> 2020
Integrated approach	Activated carbon and CaO, ion exchange resin	High removal efficiency and strong specificity	Higher economic costs	Santos <i>et al.</i> 2014; Cheng <i>et al.</i> 2017

### Physical Methods

Physical methods are usually used to remove part of the inhibitor in the pretreatment solution by physical method to reduce or eliminate its inhibitory effect, which is the simplest method of detoxification. Common methods include rotary evaporation (Llano Astuy *et al.* 2017) adsorption, extraction, and membrane filtration.

### Adsorbent Method

The adsorption method usually involves adding an adsorbent to the pretreatment liquid to combine with the inhibitor and precipitate, thereby removing the inhibitor (Llano Astuy *et al.* 2017). Activated carbon has a strong adsorption effect and low cost, so it has become one of the commonly used adsorbents. In addition, new adsorbents and cross-linked polyethyleneimine (PEI), and other adsorbents are also unique (López-Linares *et al.* 2016; Huang *et al.* 2018). The structure and excellent adsorption performance have attracted widespread attention. Ravindran and Jaiswal (2016) used activated carbon to adsorb by-products in the hydrolysate of cotton stalk after sodium hydroxide pretreatment, which reduced the total mass of furfural by 59.1%. However, the disadvantage of this treatment method is the loss of higher reducing sugars. Substances such as adsorption resin and PEI can selectively adsorb furan, fatty acid, and phenolic substances in the lignocellulose pretreatment solution, and then use the desorption mechanism to recover these substances (Carter *et al.* 2011). Deng *et al.* (2018) used PEI and polydiallyldimethylammonium chloride (pDADMAC) to adsorb and recover formic acid, acetic acid, and levulinic acid in the bagasse enzymatic hydrolysate, after dilute ammonia pretreatment, furfural, 5-HMF, and phenolic were reduced. The results showed that the

effect was the best when the pH was 4.5, and when the addition amount of PEI and pDADMAC was 15 g/L. It was able to remove 43 per of organic acids, 73 per of total phenolic compounds, and 100 per of furan aldehyde compounds. The loss of fermentable sugar was less than 10%.

### Solvent Extraction Method

The solvent extraction method employs solvent to separate the inhibitors from the fermentation broth because of the difference in the solubility of sugars and inhibitors in the extracting agent. The commonly used extractants are n-hexane, chloroform, and ethyl acetate. Studies have shown that extraction with ethyl acetate can remove peracetic acid and all furfural, vanillin, and 4-hydroxybenzoic acid in lignocellulose hydrolysate (Palmqvist and Bärbel 2000). Zhang *et al.* (2005) studied the effect of several different extractants on inhibitors, and the results showed that among the three organic solvents, n-hexane had a poor removal effect on several inhibitors, while ethyl acetate and chloroform had a higher removal effectiveness for furfural, but the removal effect on phenolic compounds was poor. This is because the polarity of furfural is less than that of phenolic compounds. As a consequence, the solubility of furfural in organic solvents such as ethyl acetate and chloroform is higher, so the removal of furfural is higher than that of phenolic substances when extracted with organic solvents. Because xylose is almost insoluble in organic solvents, extraction with organic solvents has little effect on it.

### Membrane Separation Method

The removal of various inhibitors used in nanotechnology has the characteristics of separation and low energy consumption, *etc.* (Benkun *et al.* 2012; Abels *et al.* 2013). At present, most of them are used in the removal of inhibitors in acid pretreatment solution. Brás *et al.* (2014) used a nano-separation membrane to detoxify the pretreatment solution of olive residue, and the results showed that 99 per of furan aldehydes, acetic acid, and formic acid could be removed, and the loss rate of reducing sugar reached 40%. When Jiang *et al.* (2018) used nano-separation membrane to detoxify dilute acid pretreatment solution, they found that the removal rate of inhibitors was affected by solution pH, osmotic flux, and concentration of Na<sub>2</sub>SO<sub>4</sub>. When treated with low pH and high concentration of Na<sub>2</sub>SO<sub>4</sub> for 35 min, 90 per of the inhibitors could be removed. Chen *et al.* (2020a) used reverse osmosis (RO) membrane to simultaneously concentrate sugar and remove inhibitors, and the results showed that the removal rates of furfural and acetic acid reached 51.6% and 77.7%, respectively. This method has a great application prospect in the production of bioethanol. Membrane separation technology has unique advantages in the detoxification of lignocellulosic pretreatment solution. However, the loss rate of reducing sugar is high, and the pretreatment inhibition species are complex, so it is difficult to remove all the inhibitors by single membrane separation technology. In addition, the cost of nano-separation membrane is high, so it cannot be industrialized to achieve large-scale production.

### Chemical Methods

Chemical methods mainly use chemical reagents to react with inhibitors in hydrolysate to bring about their precipitation. Alternatively, they can work by changing the pH and ionization properties of some inhibitors, so as to reduce the toxicity of inhibitors.

Commonly used chemical reagents include alkali and reducing agents. Of these, persulfate has received more study for detoxification in recent years.

### Alkaline Method

Adding excess alkaline substances to the hydrolysate to reduce inhibitors is a common alkaline detoxification method. Sodium hydroxide, ammonia, and calcium hydroxide are common alkaline detoxification agents. Alriksson *et al.* (2005) added  $\text{NH}_4\text{OH}$ ,  $\text{Ca}(\text{OH})_2$ ,  $\text{Mg}(\text{OH})_2$ ,  $\text{Ba}(\text{OH})_2$ , and  $\text{NaOH}$  to the dilute acid hydrolysate of spruce for detoxification, and compared the inhibitor removal effect. Treatment with  $\text{NH}_4\text{OH}$  can significantly reduce furfural and 5-hydroxymethyl furfural. Zhang *et al.* (2012) used calcium hydroxide to detoxify the corn stalk hydrolysate and found that the content of inhibitors in the corn stalk hydrolysate changed significantly. It was found that 38.8% furfural, 45.9 %, 5-hydroxymethyl furfural, and 3 % of total phenolic compounds were removed. Ikram *et al.* (2018) used 3 kinds of alkali, namely  $\text{NaOH}$ ,  $\text{NH}_4\text{OH}$ , and  $\text{Ca}(\text{OH})_2$ , to study the detoxification of pretreated wheat straw. When  $\text{Ca}(\text{OH})_2$  was immersed in the solution for 2 h, at  $\text{pH}=12$  and  $80\text{ }^\circ\text{C}$ , 60% of the phenolic compounds were obviously removed, and the sugar conversion was increased 2.4 times. The results of scanning electron microscopy (SEM) on the substrate after alkali pretreatment showed that the lignin cellulose structure had a great change, in which the lignin was degraded, so it was more susceptible to enzymatic hydrolysis. However, the disadvantage of alkali detoxification is that the amount of alkali is large, and neither alkali nor inhibitor can be recovered (Hamidah *et al.* 2017; Zhang *et al.* 2018).

### Reducing Agent Method

This method works by adding reducing agents to the hydrolysate to achieve the effect of detoxification. Commonly used reducing agents are sulfites and hydrogen peroxide. The reducing agent method is easy to operate, can improve the fermentation effect, and ensure that the reducing sugar in the hydrolysate is not lost, and has a good development prospect. Alriksson *et al.* (2011) conducted SHF (simultaneous hydrolysis and fermentation) experiments on pretreatment hydrolysates of spruce or bagasse treated with bisulfite and sulfite, and the results showed that the ethanol yield of spruce hydrolysate fermented by bisulfite treatment increased from  $0.2\text{ g}/(\text{L}\cdot\text{h})^{-1}$  to  $2.5\text{ g}/(\text{L}\cdot\text{h})^{-1}$ , and that of bagasse fermented ethanol yield increased from  $0.9\text{ g}/(\text{L}\cdot\text{h})^{-1}$  to  $3.9\text{ g}/(\text{L}\cdot\text{h})^{-1}$ . Soudham *et al.* (2014) used  $2.5\text{ mmol/L FeSO}_4$  and  $150\text{ mmol/L H}_2\text{O}_2$  to treat the hydrolysates of Chinese fir and found that this method could effectively remove 29 per of 5-HMF, 34 per of furfural, and 24 per of phenolic substances, and increase the ethanol yield from  $0.4\text{ g/L}$  to  $8.3\text{ g/L}$ . The use of reductant is a common method of detoxification, but the disadvantage is that the detoxification range is small, and there is low specificity.

### Persulfate Method

Persulfate, which is a strong oxidizer, is relatively stable at room temperature and soluble in water (Cong *et al.* 2015). Persulfate can produce the sulfate radical, which can selectively oxidize and degrade phenol material. For these reasons, this technique is often used in the environmental engineering field containing phenol wastewater treatment. The treatment of phenol-containing wastewater in the engineering field is similar to treatment of lignocellulose degradation products. In recent years, the persulfate method has been used as a new technology for the detoxification of hydrolysate. UV (Gao *et al.* 2012), heat (Liang *et al.* 2003), acids, bases, and transition metals (Yang *et al.* 2009) are all effective in

activating persulfates. Compared with  $\text{OH}^-$ ,  $\text{S}_2\text{O}_8^{2-}$  has a wider pH range and longer duration, so it has a broad application prospect in the degradation of hydrolysate inhibitors (Wu *et al.* 2020). Rong *et al.* (2016) and others used a new type of detoxification technology-heat activated persulfate advanced oxidation to remove the typical inhibitors in the production process of bioethanol (vanillin, syringaldehyde, 4-hydroxybenzaldehyde, vanillic acid, syringic acid, and 4-hydroxybenzoic acid). Studies have shown that the effect of thermally activated persulfate oxidative degradation products is significant, and the removal percentages of vanillin, 4-hydroxybenzaldehyde, vanillic acid, 4-hydroxybenzoic acid, and syringic acid all reach 100% within 1 h. Similarly, the removal of syringaldehyde can reach 100% within 2 h. Zhou *et al.* (2021) used activated persulfate to degrade phenols, and the efficiency reached 98.2 per within 120 minutes. The main mechanism is that the sulfate radical reacts with the inhibitor to degrade it into small non-toxic substances.

### Biological Methods

Biological methods usually use microorganisms or enzymes to act on the inhibitors in the hydrolysate, and then they react with them to produce low-toxicity or non-toxic substances, so as to achieve the purpose of improving the fermentation efficiency. Biological methods are generally divided into two categories: microbial and enzymatic methods. The advantages of biological methods are specificity, mild conditions, and no introduction of new impurities.

### Enzymatic Detoxification

Saravanakumar *et al.* (2016) used a new class of material – nanofibers – to immobilize laccase and found that furfural, acetosyringone, and coniferous aldehyde in the lignocellulose hydrolysate can be completely removed by reacting at 40 °C for 36 hours. The sugar loss is low. Tramontina *et al.* (2020) added peroxidase and superoxide dismutase to the bagasse hemicellulose hydrolysate for detoxification. The results showed that butanol was produced by the fermentation of the bacterium *Clostridium* spp. and ethanol was produced by the action of yeast. Compared with the hydrolyzed solution without detoxification, it increased by 24 times and 2.4 times, respectively. Studies have found that the detoxification effect of laccase is related to the time it is added (Jurado *et al.* 2009; Oliva-Taravilla *et al.* 2015).

### Microbial Detoxification Method

White rot fungi (WRF) is a commonly used group of microorganisms suitable for detoxification. Specifically, WRF usually degrades furfural, acids, and aromatic aldehyde compounds (Bulter *et al.* 2003; Hasunuma *et al.* 2011). Nichols *et al.* (2008) added the fungus *Coniochaeta ligniaria* NRRL30616 to the dilute acid hydrolysate of corn stalk to removed the toxic components. Quantitative analysis showed that 5-hydroxymethyl furfural, furfural, and phenolics were effectively removed, and only small amounts of glucose (usually 2.5 g/L or less) were lost.

A breakthrough was made in the study of inhibitor-tolerant strains for maintaining efficient saccharification in the presence of multiple inhibitors. Fonseca *et al.* (2011) treated bagasse hydrolyzate with the strain of *Issatchenkia occidentalis* (CCTCC M 206097) and found that the concentration of reducing sugar did not decrease after 24 h of detoxification, while the concentrations of syringaldehyde, ferulic acid, furfural, and 5-HMF decreased by 62%, 67%, 33%, and 85%, respectively. Other studies have found that

strain Y-50049, induced by aldehydes and 5-HMF, is activated and expressed in ZWF1 to produce NADPH, which can assist aldehyde reductase to reduce furfural and 5-HMF and can remove furfural aldehydes (Todhanakasem *et al.* 2018). With the rapid development of modern molecular biology techniques, it is possible to breed and screen out the strains with high efficiency and strong tolerance, and it is possible to use genetic engineering methods to clone the genes of virus-free strains and construct a variety of engineering strains with different types and functions. This is a new trend of using microorganisms.

### Compound Detoxification Methods

In recent years, researchers have adopted a combined detoxification method, which combines several single methods for detoxification, achieving better detoxification effects and obtaining more fermentation products. There are a variety of inhibitors in the lignocellulose pretreatment solution. The structural components are complex, and each has a synergistic inhibitory effect. Using a single detoxification method cannot achieve the expected effect, and each method has its own shortcomings. Yücel and Aksu (2015) added activated carbon, activated carbon for beet meal, and fly ash to the beet meal hydrolysate for detoxification. Studies have shown that in the presence of CaO, activated carbon has a better adsorption effect on phenols and furan compounds, and fly ash can remove a large number of furan compounds. In addition, Santos *et al.* (2014) combined ion exchange resin with activated carbon as a new method for removing inhibitors. At a temperature of 30 °C and a flow rate of 2.5 VB/h, the concentration of most furfural, 5-HMF, and phenols decreased. Similarly, Cheng *et al.* (2017) used organic acids to detoxify the pretreatment liquid by activated carbon and ion exchange resin, and the results showed that the yield of bacterial cellulose reached 2.86 g/L. Tomek *et al.* (2015) combined enzymes and liquid-liquid extraction to achieve detoxification of inhibitors in the pretreatment solution, which can effectively remove inhibitors and improve enzymatic hydrolysis and fermentation efficiency.

### SUMMARY AND PROSPECTS

The use of lignocellulose to produce biofuels such as methanol and ethanol has become an industry trend, and the implementation of such technology is expected to alleviate the energy shortage in the world today. Seeking effective pretreatment methods and detoxification methods is the core of improving the utilization rate of lignocellulose. In order to improve the utilization rate of wood fiber, breakthroughs can be made from the following aspects:

1. Explore more effective pretreatment methods, or develop new reagents to increase the degradation rate of wood fiber while producing as few inhibitors as possible;
2. Most of the inhibitors in the existing pretreatment process have been determined, but their inhibitory mechanism on enzymes and cellulose has not been fully elucidated, so more in-depth research will be carried out in this part in the future;
3. In addition, the effective removal of inhibitors in the pretreatment solution is also an important aspect of research and development. There are many types of inhibitors. The existing detoxification methods cannot completely remove the inhibitors and cause loss of reducing sugars. Therefore, it is necessary to develop materials for efficiently

removing inhibitors or use genetic engineering, cell engineering, *etc.* Modern biotechnology has genetically modified fermenting microorganisms to screen out microorganisms with higher fermentation tolerance, which can maximize the conversion and utilization of biomass resources.

## ACKNOWLEDGMENTS

This work was funded by the National Key Research and Development Program of China (No. 2019YFB1503802) and Scientific Research Project of Department of Education of Hunan Province (No.20K144).

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Article submitted: July 28, 2021; Peer review completed: October 9, 2021; Revised version received: December 8, 2021; Accepted: December 9, 2021; Published: December 15, 2021.

DOI: 10.15376/biores.17.1.Luo